Results of Proficiency Test Liquefied Butane Analysis May 2010

Organised by: Institute for Interlaboratory Studies Spijkenisse, the Netherlands

Author:Dr. R.G. VisserCorrector:Mr. Ivar KoorenReport:iis10S02B

July 2010

## CONTENTS

1	INTRODUCTION	3
2	SET UP	3
2.1	QUALITY SYSTEM	3
2.2	PROTOCOL	3
2.3	CONFIDENTIALITY STATEMENT	4
2.4	SAMPLES	4
2.5	STABILITY OF THE SAMPLES	5
2.6	ANALYSES	5
3	RESULTS	5
3.1	STATISTICS	5
3.2	GRAPHICS	6
3.3	Z-SCORES	6
4	EVALUATION	7
4.1	EVALUATION PER TEST/COMPONENT	7
4.2	PERFORMANCE EVALUATION FOR THE GROUP OF LABORATORIES	10
4.3	DISCUSSION	11

## Appendices:

1.	Data and statistical results	12
2.	Additional details	26
3.	List of participants	27
4.	Abbreviations and literature	28

## 1 INTRODUCTION

During the last years, with increasing frequency, requests were received by iis from laboratories that participated in the iis PT program, to organize also a proficiency test for the Liquefied Butane Analysis. Beginning 2008, iis started an investigation for the feasibility of such a PT. Because iis has limited gas-handling facilities in place to prepare gas samples, Scott Specialty Gases (Breda, the Netherlands) was contacted. This company is fully equipped and has a broad experience in the preparation of synthetic Liquefied Butane samples for PT purposes. Together with this company, it was decided to organize a first proficiency study for Liquefied Butane (composition only) in 2009.

This interlaboratory study was repeated in 2010, in which now 24 laboratories from 16 different countries have participated. See appendix 3 for a list of participants in alphabetical country order.

In this report the results of the 2010 proficiency test on Liquefied Butane are presented and discussed.

### 2 SET UP

The Institute for Interlaboratory Studies (iis) in Spijkenisse, The Netherlands, was the organizer of this proficiency test.

To optimise the costs for the participating laboratories, it was decided to prepare one Liquefied Butane mixture. The mixture was divided over a batch of 30 cylinders.

The cylinder size is a cost-effective two-litre cylinder with dip tube device.

Each cylinder was uniquely numbered. The limited cylinder size is chosen to optimise transport and handling costs.

Participants were requested to report rounded and unrounded results. The unrounded results were preferably used for statistical evaluation.

#### 2.1 QUALITY SYSTEM

The Institute for Interlaboratory Studies in Spijkenisse, the Netherlands, has implemented a quality system based on ISO guide 43, ISO 17043:2010 and ILAC-G13:2007. This ensures 100% confidentially of participant's data. Also customer's satisfaction is measured on regular basis by the distribution of questionnaires.

## 2.2 PROTOCOL

The protocol followed in the organisation of this proficiency test was the one as described for proficiency testing in the report 'iis Interlaboratory Studies: Protocol for the Organisation, Statistics and Evaluation' of January 2010 (iis-protocol, version 3.2).

### 2.3 CONFIDENTIALITY STATEMENT

All data present in this report must be regarded as confidential and for use by the participating companies only. Disclosure of the information in this report is only allowed by means of the entire report. Use of the contents of this report for third parties is only allowed by written permission of the Institute for Interlaboratory Studies. Disclosure of the identity of one or more of the participating companies will be done only after receipt of a written agreement of the companies involved.

### 2.4 SAMPLES

In this proficiency test only one sample was used. A batch of two-litre cylinders with artificial Liquefied Butane mixture was prepared and tested for homogeneity by Scott Specialty Gases (Breda, the Netherlands) in conformance with ISO 6143 and ISO Guide 35. In total one batch of 30 cylinders was prepared (lot 79022) on April 29, 2010. Each cylinder was uniquely numbered. One cylinder was tested 10 times, on 10 following days, to check the stability. The remaining 29 cylinders were all tested in threefold to check the homogeneity of the batch. By ANOVA analysis on the test results in accordance with ISO 6143 the in-between bottle standard deviation was calculated. The repeatability values (r) were calculated per component by multiplication of the respective standard deviation by 2.8. Subsequently the calculated repeatabilities were compared with 0.3 times the corresponding target reproducibilities in agreement with the procedure of ISO 13528, Annex B2 in the next table:

Parameter	conc. in %mol/mol	r(observed) in %mol/mol	0.3 X R(D2163) in %mol/mol
Propane	1.947	0.056	0.068
Propylene	1.449	0.050	0.054
n-Butane	8.134	0.192	0.285
1,3-Butadiene	0.897	0.009	0.032
iso-Butylene	4.026	0.036	0.136
1-Butene	4.991	0.057	0.170
trans-2-Butene	2.005	0.029	0.075
cis-2-Butene	1.017	0.020	0.037
iso-Pentane	0.710	0.017	0.025
iso-Butane	74.824	0.264	0.360

Table 1: homogeneity test results

The calculated repeatabilities are each less than 0.3 times the corresponding reproducibility of the reference method ASTM D2163. Therefore, homogeneity of the subsamples #10BU was assumed.

To each of the participating laboratories one 2L cylinder was sent on May 10, 2010.

#### 2.5 STABILITY OF THE SAMPLES

The ten test results of the cylinder tested at ten subsequent days were identical. Also, Scott Specialty Gases (Breda, the Netherlands) declares that the prepared sample cylinders have a shelf life of at least 6 months. This is sufficient for the proficiency testing purposes.

#### 2.6 ANALYSES

The participants were asked to determine: Propane, Propylene, n-Butane, 1,3-Butadiene, iso-Butylene, 1-Butene, trans-2-Butene, cis-2-Butene, iso-Pentane, iso-Butane, Molar Mass, Relative Density and Absolute and Relative Vapour pressure. Also some method details were requested to be reported. To get comparable results a detailed report form, on which the units were prescribed, was sent together with each set of samples. Also a letter of instructions and a SDS were added to the package.

Participants are also requested to send a remark if other components were found e.g. Helium or/and Pentane.

#### 3 RESULTS

During four weeks after sample despatch, the results of the individual laboratories were gathered. The original results are tabulated per determination in the appendix 1 of this report. The laboratories are presented by their code numbers.

Directly after the deadline the available results were screened for suspect data. A result was called suspect in case the Huber Elimination Rule (a robust outlier test) found it to be an outlier. The laboratories that produced these suspect data were asked to check the results. Additional or corrected data are put under 'Remarks' in the result tables in appendix 1. Results that came in after deadline were not taken into account in the screening for suspect data and thus these participants were not requested for checks.

#### 3.1 STATISTICS

The protocol followed in the organisation of this proficiency test was the one as described for proficiency testing in the report 'iis Interlaboratory Studies: Protocol for the Organisation, Statistics and Evaluation' of January 2010 (iis-protocol, version 3.2).

For the statistical evaluation the *unrounded* (when available) figures were used instead of the rounded results. Results reported as '<...' or '>...' were not used in the statistical evaluation.

First the normality of the distribution of the various data sets per determination was checked by means of the Lilliefors-test. After removal of outliers this check was repeated. In case a data set does not have a normal distribution, the results of the statistical evaluation should be used with due care.

In accordance with ISO 5725 (1986 and 1994) the original results per determination were submitted subsequently to Dixon and Grubbs outlier tests. Outliers are marked by D(0.01) for

the Dixon test and by G(0.01) or DG(0.01) for the Grubbs test. Stragglers are marked by D(0.05) for the Dixon test and by G(0.05) or DG(0.05) for the Grubbs test. Both outliers and stragglers were not included in the calculations of the averages and the standard deviations.

Finally the reproducibilities were calculated from the standard deviations by multiplying these with a factor of 2.8.

### 3.2 GRAPHICS

In order to visualize the data against the reproducibilities from literature, Gauss plots were made, using the sorted data for one determination (see appendix 1). On the Y-axis the reported analysis results are plotted. The corresponding laboratory numbers are under the X-axis.

The straight horizontal line presents the consensus value (a trimmed mean). The four striped lines, parallel to the consensus value line, are the +3s, +2s, -2s and -3s target reproducibility limits of the selected standard. Outliers and other data, which were excluded from the calculations, are represented as a "x". Accepted data are represented as a triangle. Furthermore, Kernel Density Graphs were made. This is a method for producing a smooth density approximation to a set of data that avoids some problems associated with histograms (see appendix 3; nr.13 and 14).

## 3.3 Z-SCORES

To evaluate the performance of the participating laboratories the z-scores were calculated. As it was decided to evaluate the performance of the participants in this proficiency test (PT) against the literature requirements, e.g. ASTM, EN-, ISO-, IP reproducibilities, the z-scores were calculated using a target standard deviation. This target standard deviation was calculated from the literature reproducibility by division with 2.8. The z-scores were calculated according to:

z(target) = (result - average of PT) / target standard deviation

The z(target) scores are listed in the result tables in appendix 1.

Absolute values for z<2 are very common and absolute values for z>3 are very rare. Therefore the usual interpretation of z-scores is as follows:

|z| < 1 good 1 < |z| < 2 satisfactory 2 < |z| < 3 questionable 3 < |z| unsatisfactory

## 4 EVALUATION

In this proficiency test several problems were encountered with sample transport. Due to customs problems two cylinders did not reach the laboratory in time to test the cylinder and to report results to be included in the final report. In total six laboratories reported the test results after the final reporting date. Not all laboratories were able to report all test results requested.

Two laboratories appeared to have some problems. Six test results (=60%) reported by laboratory 317 appeared to be statistical outliers and because all test results of one laboratory are correlated, the remaining four test results of lab 317 were excluded manually from the statistical analysis.

Because 14 laboratories reported both results in %mol/mol as well as in %M/M, it has been possible to check the calculations of these 14 laboratories. A good correctation between the results reported in %mol/mol and the results reported in %M/M is to be expected. Thus it was noticed that laboratory 1117 obviously had made a calculation error. Fortunately the laboratory was able to locate and correct the error and to report revised test results. Also, one test result of laboratory 1634 (for iso-Butylene) was deviating, see page 16. Some other (small) deviations may be explained by the reporting of test results too far rounded.

In total 22 participants reported 263 numerical results. Observed were 20 outlying results, which is 7.6% of the numerical results. In proficiency studies outlier percentages of 3% - 7.5% are quite normal.

#### 4.1 EVALUATION PER TEST/COMPONENT

In this section the results are discussed per component. The methods, which are used by the various laboratories, are taken into account for explaining the observed differences when possible and applicable. These methods are also in the tables together with the original data. The abbreviations, used in these tables, are listed in appendix 3.

All original data sets proved to have a normal distribution, except for the Molar Mass and Absolute Vapour Pressure results.

Because the majority of the participating laboratories used ASTM D2163 as test method, it was decided to use the reproducibilities of this test method as target reproducibilities, and to mention the reproducibilities of EN27941 (identical to IP 405 and ISO 7941) for reference only. Regretfully in the last version ASTM D2163:07 only repeatabilities, but no reproducibilies are mentioned. Therefore the precision data from the previous version ASTM D2163:96 were used.

<u>Propane</u>: The determination of this component may be problematic. Two statistical outliers were detected and the calculated reproducibility, after exclusion of the statistical outliers, is not in agreement with the requirements of ASTM D2163:96. However, the calculated reproducibility is in agreement with the less strict reproducibility of EN27941 (identical to IP 405 and ISO 7941).

- <u>Propylene:</u> The determination of this component may be problematic. Two statistical outliers were detected and the calculated reproducibility, after exclusion of the statistical outliers, is not at all in agreement with the requirements of ASTM D2163:96. However, the calculated reproducibility is in agreement with the less strict reproducibility of EN27941 (identical to IP 405 and ISO 7941).
- <u>n-Butane:</u> No large analytical problems were observed. Two statistical outliers were detected. However, the calculated reproducibility, after exclusion of the statistical outliers, is in full agreement with the requirements of ASTM D2163:96 and with the reproducibility of EN27941 (identical to IP 405 and ISO 7941).
- <u>1,3-Butadiene:</u> The determination of this component may be problematic. The calculated reproducibility, after exclusion of the statistical outlier, is not in agreement with the requirements of ASTM D2163:96 nor with the reproducibility of EN27941 (identical to IP 405 and ISO 7941).
- iso-Butylene: No large analytical problems were observed. Two statistical outliers were detected. However, the calculated reproducibility, after exclusion of the statistical outliers, is in full agreement with the requirements of ASTM D2163:96 and with the reproducibility of EN27941 (identical to IP 405 and ISO 7941).
- <u>1-Butene:</u> No analytical problems were observed. No statistical outliers were detected. And the calculated reproducibility is in agreement with the requirements of ASTM D2163:96 and with the reproducibility of EN27941 (identical to IP 405 and ISO 7941).
- trans-2-Butene: The determination of this component may be problematic. The calculated reproducibility, after exclusion of the statistical outlier, is not in agreement with the requirements of ASTM D2163:96. However, the calculated reproducibility is in agreement with the less strict reproducibility of EN27941 (identical to IP 405 and ISO 7941).
- <u>cis-2-Butene:</u> The determination of this component may be problematic. The calculated reproducibility, after exclusion of the statistical outlier, is not in agreement with the requirements of ASTM D2163:96. However, the calculated reproducibility is in agreement with the less strict reproducibility of EN27941 (identical to IP 405 and ISO 7941).
- iso-Pentane:The determination of this component may be problematic. Three<br/>statistical outliers were detected and the calculated reproducibility, after<br/>exclusion of the statistical outliers, is not in agreement with the<br/>requirements of ASTM D2163:96. However, the calculated

reproducibility is in agreement with the less strict reproducibility of EN27941 (identical to IP 405 and ISO 7941).

iso-Butane: The determination of this component may be problematic. No statistical outliers were detected. However, the calculated reproducibility is not at all in agreement with the requirements of ASTM D2163:96, nor with the less strict reproducibility of EN27941 (identical to IP 405 and ISO 7941). The data set seems to be bimodally divided with one maximum around 74.5 %V/V (13 test results) and another maximum around 75.8 %V/V (9 test results).

<u>Molar Mass:</u> This calculated parameter may be problematic. The results vary over a large range from 56.69 - 57.73 and two statistically significant outliers were present (in 9 test results). See also the discussion in 4.3.

<u>Relative Density</u>: This calculated parameter may be problematic. The results vary over a range from 0.5674 - 0.5700 and one statistically significant outlier was present (in 14 test results). See also the discussion in 4.3.

- <u>Abs. Vapour Pres.</u>: This calculated parameter may be problematic. The results vary over a large range (72.0 76.4 psi) and one statistically significant outlier was observed. See also the discussion in 4.3.
- <u>Rel. Vapour Pres.</u>: This calculated parameter may be problematic. The results vary over a large range (58.0 60.6 psi) and one statistically significant outlier was observed. See also the discussion in 4.3.

#### 4.2 PERFORMANCE EVALUATION FOR THE GROUP OF LABORATORIES

A comparison has been made between the reproducibility as declared by the relevant standard and the reproducibility as found for the group of participating laboratories. The average results per sample, calculated reproducibilities and reproducibilities, derived from literature standards (in casu ASTM D2163 and EN27941/ISO7941/IP405) are compared in the next table.

Parameter	unit	n	cons. value	2.8 * sd	R(D2163)	R(EN27941) liqinj.	R(EN27941) liqinj.
					in <b>%mol</b>	in %mol	in % <b>M/M</b>
Propane	%mol/mol	20	1.973	0.342	0.227	0.767	1
Propylene	%mol/mol	19	1.279	0.281	0.147	0.732	1
n-Butane	%mol/mol	20	8.245	0.811	0.949	1.011	1
1,3-Butadiene	%mol/mol	19	0.941	0.150	0.108	0.941	1
iso-Butylene	%mol/mol	19	3.951	0.329	0.454	0.976	1
1-Butene	%mol/mol	21	4.950	0.606	0.569	0.976	1
trans-2-Butene	%mol/mol	21	2.177	0.286	0.251	0.976	1
cis-2-Butene	%mol/mol	21	1.072	0.159	0.123	0.976	1
iso-Pentane	%mol/mol	19	0.715	0.106	0.082	1.255	1
iso-Butane	%mol/mol	20	74.904	1.907	1.200	1.516	1.5
Molar Mass	g/mol	7	57.41	0.29	n/a	n/a	n/a
Relative Density		13	0.5692	0.010	n/a	n/a	n/a
Abs. Vapour pres.	psi	10	73.19	1.74	n/a	n/a	n/a
Rel. Vapour pres.	psi	10	58.28	1.47	n/a	n/a	n/a

Table 2: Performance of the group in comparison with the target reproducibilities

Without further statistical calculations it can be concluded that for many components there is not a good compliance of the group of participating laboratories with the relevant standard. The problematic components/tests have been discussed in paragraph 4.1.

## 4.3 DISCUSSION

Because several of the reproducibility requirements of ASTM D2163 differ significantly from the reproducibility requirements of EN27941 (for liquid injection), the outcome of the evaluations will be strongly dependent on the target test method selected for the evaluation.

The consensus values as determined in this PT are compared with the average values from the homogeneity testing by Scott Specialty Gases in the following table. From this comparison it is clear that most consensus values as determined in this PT are well in line with the values as determined during the preparation of the gas cylinders except for Propylene (z-score in bold). No explanation can be given for this observation.

Parameter	Average values by Scott Specialty Gases in %mol/mol	Consensus values from participants results in %mol/mol	Absolute differences in %mol/mol	z-score
Propane	1.947	1.973	+0.026	+0.32
Propylene	1.449	1.279	-0.170	-3.16
n-Butane	8.134	8.245	+0.111	+0.32
1,3-Butadiene	0.897	0.941	+0.044	+1.11
iso-Butylene	4.026	3.951	-0.075	-0.46
1-Butene	4.991	4.950	-0.041	-0.20
trans-2-Butene	2.005	2.177	+0.172	+1.92
cis-2-Butene	1.017	1.072	+0.055	+1.28
iso-Pentane	0.710	0.715	+0.005	+0.18
iso-Butane	74.824	74.904	+0.080	+0.19

Table 3: comparison of consensus values with values determined by Scott Specialty Gases

In total 8 laboratories reported the presence of some n-pentane (0.0035 %mol/mol with sd = 0.0004 %mol/mol), a component probably present as impurity in one or more of the pure components that were used to prepare the iso-Butane mixture. Also two laboratories reported the presence of some helium (0.45 – 1.4 %mol/mol). See appendix 2.

In principle no additional spread should be introduced when applying a calculation on the reported component concentrations. However, in practice a significant additional uncertainty is added. See the differences between the values from the results as reported by the participating laboratories (each using its own calculation procedure) and the values as calculated by iis using one calculation procedure for each set of laboratory test results. For the calculation of the Molar Mass, Relative Density and Vapour Pressure several standardized methods are available, e.g. ASTM D2421 for the interconversion of the units to gas-volume, liquid-volume or mass basis. Also different methods for the calculation of the Vapour Pressure do exist. In ISO 8973 (identical to IP432) the Vapour Pressure is calculated from the <u>mole fraction</u> per component and a Vapour Pressure is calculated from the <u>liquid volume percentage</u> per component and a Vapour Pressure factor of that component (given for only several components).

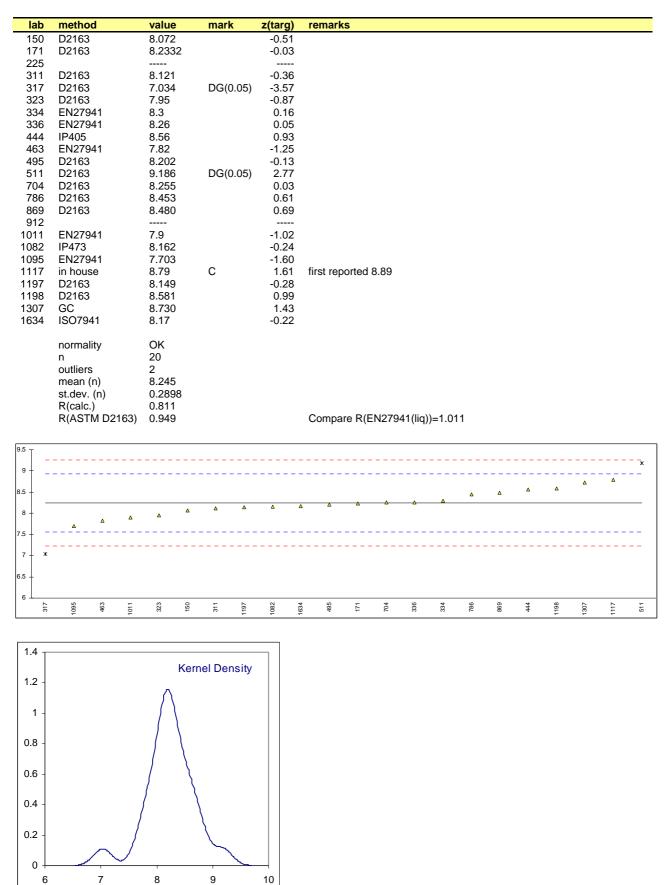
# Determination of Propane; results in %mol/mol

	mination of Pro														
lab	method	value	mark	z(targ)	remarks										
150	D2163	1.989		0.20											
171	D2163	1.8036		-2.09											
225	Datas														
311	D2163	1.982	0(0.04)	0.11											
317	D2163	2.867	G(0.01)	11.03											
323	D2163	2.03		0.70											
334	EN27941	2.0		0.33											
336	EN27941	1.92		-0.65											
444	IP405	1.78		-2.38											
463 495	EN27941 D2163	2.09 1.902		1.44 -0.87											
493 511	D2163	2.145		2.12											
704	D2163 D2163	1.933		-0.49											
786	D2163	2.024		0.63											
869	D2163	1.951		-0.27											
912	D2100														
1011	EN27941	1.9		-0.90											
1082	IP473	1.921		-0.64											
1095	EN27941	1.922		-0.63											
1117	in house	2.14	С	2.06	first reporte	ed 1.25									
1197	D2163	2.166	C	2.38	motropolit										
1198	D2163	2.127		1.90											
1307	GC	1.732		-2.97											
1634	ISO7941	1.14	G(0.05)	-10.27											
			- (0.00)												
	normality	OK													
	n	20													
	outliers	2													
	mean (n)	1.973													
	st.dev. (n)	0.1222													
	R(calc.)	0.342													
	R(ASTM D2163)	0.227			Compare F	R(EN2794	41(liq)	)=0.76	7						
<sup>3</sup> T															
															*
2.8 -															*
2.8 - 2.6 -															*
2.8 - 2.6 - 2.4 -															×
2.8 - 2.6 - 2.4 - 2.2							= = = =			- <u>-</u>	— — <u>A</u> — —	<u>-</u>	- Δ· - ·		*
2.8 - 2.6 - 2.4 -									 Δ	Δ		<u>-</u>	Δ – Ξ		*
2.8 - 2.6 - 2.4 - 2.2				A	<u> </u>					Δ		<b>_</b>	<b>•</b>		*
2.8 - 2.6 - 2.4 - 2.2 2		A	Δ Δ	Δ Δ					Δ	Δ	<u>A</u>	<u>a</u>	Δ		*
2.8 - 2.6 - 2.4 - 2.2 2.2 1.8 1.6 -	<u>A</u> <u>A</u> <u>A</u>	Δ Δ	<u> </u>	Δ 4	Δ Δ Δ			Δ 	Δ	Δ	<u>a</u>	<u>A</u>			*
2.8 - 2.6 - 2.4 - 2.2 2.4 - 2.2 1.8 1.6 - 1.4 -	<u>-</u> <u>-</u>	Δ Δ 	Δ Δ 	Δ 4	Δ Δ			 	Δ	Δ	- <u>-</u>	<u>a</u>			x
2.8 - 2.6 - 2.4 - 2.2 2.2 1.8 1.6 - 1.4 - 1.2			<u> </u>	4	Δ Δ Δ			 	 		<u>A</u>	<u>A</u>			x
2.8 - 2.6 - 2.4 - 2.2 2.8 - 1.8 1.6 - 1.4 - 1.2 1				A 4		<u>A</u>	2 				- <u> </u>				
2.8 - 2.6 - 2.4 - 2.2 2.2 1.8 1.6 - 1.4 - 1.2	1307 444 177	1011 495 • • • • •	336 7 7 7 7 7 7 7 7 7 7 7 7 7 7 7 7 7 7 7	1085 704 704		150	334	4	323	463	<del>-</del>		511	1197	317
2.8 - 2.6 - 2.4 - 2.2 2.8 - 1.8 1.6 - 1.4 - 1.2 1	1307 44 4 			1085 704 704		150 	334					<b>P</b>	511	1197	
$ \begin{array}{cccccccccccccccccccccccccccccccccccc$	1007 444 7 7 7 7 7 7 7 7 7 7 7 7			1085 704 704	5 88 5 33 88 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5	150 T	334				98 		5	1197	
2.8 - 2.6 - 2.4 - 2.2 2.8 - 1.8 1.6 - 1.4 - 1.2 1	1307 444 171 4 4 4 4 4			20 20 20 20 20 20 20 20 20 20 20 20 20 2	<b>A A</b> 	150	334				110 110 110 110 110 110 110 110 110 110	1117	51	2611	
$ \begin{array}{cccccccccccccccccccccccccccccccccccc$	1307 1444 171	1011 486	336 1082		<b>△ △</b>  	150	334				110 110 110 110 110 110 110 110 110 110	111 111 111	51	197	
$ \begin{array}{c} 2.8 \\ 2.6 \\ 2.4 \\ 2.2 \\ - \\ 2 \\ - \\ 1.8 \\ - \\ 1.6 \\ 1.4 \\ 1.2 \\ - \\ 1 \\ - \\ \frac{7}{2} \\ $	1307 1307 444 171	1011 486			алан алан алан алан алан алан алан алан	150	334				86 138 	1112 1112	51	1197	
$ \begin{array}{cccccccccccccccccccccccccccccccccccc$	1307 1307 144 141	1011 486	336 1082		2 68 5	190	334				89 10 10 10 10 10 10 10 10 10 10 10 10 10	1117	51	197	
$ \begin{array}{c} 2.8 \\ 2.6 \\ 2.4 \\ 2.2 \\ - \\ 2 \\ - \\ 1.8 \\ - \\ 1.6 \\ 1.4 \\ 1.2 \\ - \\ 1 \\ - \\ \frac{7}{2} \\ $	1307 1307 444 171	1011 486	336 1082		2 09 12 2 09 12 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1	150	334				 − 000 000 000 000 000 000 000	1117	51	1197	
$ \begin{array}{cccccccccccccccccccccccccccccccccccc$	1307 1444 171 191 191 191 191 191 191 191 191 191	1011 486	336 1082		<b>A A</b> <b>A A</b> <b>A A</b> <b>A A</b> <b>B A</b> <b>A</b> <b>A</b> <b><b>A</b> <b><b>A</b> <b><b>A</b> <b><b>A</b> <b><b>A</b> <b><b>A</b> <b>A</b> </b></b></b></b></b></b>	150	334				1188 <b>-</b>	1117	51	1197	
$ \begin{array}{c} 2.8 \\ 2.6 \\ 2.4 \\ 2.2 \\ - \\ 2 \\ - \\ 1.8 \\ - \\ 1.6 \\ 1.4 \\ 1.2 \\ - \\ 1 \\ - \\ \frac{7}{2} \\ $	1307 144 171 171	1011 486	336 1082		2. <u>2</u> <u>2</u> <u>2</u> 2. <u>2</u> <u>2</u> 3. <u>4</u> 3. <u>4</u> 5. <u>5</u> 5. <u></u>	150	334				1988 1988 1988 1988 1988 1988 1988 1988	1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1	51	1197	
$ \begin{array}{cccccccccccccccccccccccccccccccccccc$	1307 1307 171 171	1011 486	336 1082			150	334				 	117	51	1197	
$ \begin{array}{cccccccccccccccccccccccccccccccccccc$	1307 144 171 184 184 184 184 184 184 184 184 184 18	1011 486	336 1082			150	334						15 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2	1197	
$ \begin{array}{cccccccccccccccccccccccccccccccccccc$	100 100 100 100 100 100 100 100 100 100	1011 486	336 1082		<b>A A</b> 33 88 33 88 34 88		334				  	111	1 <u>5</u>	1197	
$ \begin{array}{cccccccccccccccccccccccccccccccccccc$	1307 144 171 171	1011 486	336 1082		<b>A A</b> 	156 7	334				   	111	12	1197	
$\begin{array}{c} 2.8 \\ 2.6 \\ 2.4 \\ 2.2 \\ 2.4 \\ 2.2 \\ - \\ 1.8 \\ - \\ 1.6 \\ 1.4 \\ 1.2 \\ - \\ 1 \\ \frac{1}{5} \\ \frac{1}{5} \\ 2.5 \\ - \\ 2 \\ - \\ 1.5 \\ - \end{array}$		1011 486	336 1082			100	34				198 198 198 198 198 198 198 198 198 198	1117	51	2611 2611	
$ \begin{array}{cccccccccccccccccccccccccccccccccccc$	1307 1307 144 171 171	1011 486	336 1082		Δ Δ Δ 	100	34				<u>-</u> <u>-</u> 	2111	51	1197	
$\begin{array}{c} 2.8 \\ 2.6 \\ 2.4 \\ 2.2 \\ 2.4 \\ 2.2 \\ - \\ 1.8 \\ - \\ 1.6 \\ 1.4 \\ 1.2 \\ - \\ 1 \\ \frac{1}{5} \\ \frac{1}{5} \\ 2.5 \\ - \\ 2 \\ - \\ 1.5 \\ - \end{array}$	1307 144 171 144 171	1011 486	336 1082		<b>A A A A A A A A A A</b>	150	334				1198 	1117	51	1197	
$ \begin{array}{cccccccccccccccccccccccccccccccccccc$	1307 1307 144 171 191 191 191 191 191 191 191 191 191	1011 486	336 1082		<b>A A</b> <b>A A A</b> <b>A A A</b> <b>A A A</b> <b>A A A A</b> <b>A A A A A A</b> <b>A A A A A A A A A A</b>	150	334				1188 	1117	51	1197	
$\begin{array}{c} 2.8 \\ 2.6 \\ 2.4 \\ 2.2 \\ 2.4 \\ 2.2 \\ - \\ 1.8 \\ - \\ 1.6 \\ 1.4 \\ 1.2 \\ - \\ 1 \\ \frac{1}{5} \\ \frac{1}{5} \\ 2.5 \\ - \\ 2 \\ - \\ 1.5 \\ - \end{array}$	1307 144 171 171 191 197	1011 486	336 1082		<b>A A</b> <b>3</b> <b>3</b> <b>3</b> <b>4</b> <b>5</b> <b>6</b> <b>8</b> <b>6</b> <b>7</b> <b>7</b> <b>7</b> <b>7</b> <b>7</b> <b>7</b> <b>7</b> <b>7</b>	120	334					1117	51 51	1197	
$ \begin{array}{cccccccccccccccccccccccccccccccccccc$		1011 486	336 1082			150	334					1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1	51	1197	
$ \begin{array}{cccccccccccccccccccccccccccccccccccc$	1307 1307 144 171	1011 486	336 1082			150	334				  	117	51	1197	
$ \begin{array}{cccccccccccccccccccccccccccccccccccc$		For the second s	mel Density			150	33.4				<u>-</u>		2 <u>1</u>	1197	
$ \begin{array}{cccccccccccccccccccccccccccccccccccc$		1011 486	336 1082			150	334				4 		10 10 10 10 10 10 10 10 10 10 10 10 10 1		

# Determination of Propylene; results in %mol/mol

lak	we odde o al			-((+ - + - + - + - + - + - + - + - + - +											
lab 150	method D2163	value 1.319	mark	<b>z(targ)</b> 0.74	remarks	5									
171	D2163	1.2319		-0.89											
225															
311	D2163	1.337	O(0,04)	1.07											
317 323	D2163 D2163	2.049 1.42	G(0.01)	14.37 2.62											
334	EN27941	1.42		0.38											
336	EN27941	1.11		-3.16											
444	IP405	1.17		-2.04											
463	EN27941	1.37		1.69											
495 511	D2163 D2163	1.262 1.428		-0.33 2.77											
704	D2163	1.428		0.09											
786	D2163	1.336		1.06											
869	D2163	1.265		-0.27											
912	EN07044														
1011 1082	EN27941 IP473	1.2 1.286		-1.48 0.12											
1095	EN27941	1.104		-3.27											
1117					co-elutic	on with is	so-Buta	ine							
1197	D2163	1.411		2.46											
1198	D2163	1.341		1.15											
1307 1634	GC ISO7941	1.134 0.59	G(0.05)	-2.71 -12.87											
1001		0.00	0(0.00)	12.07											
	normality	OK													
	n outliere	19													
	outliers mean (n)	2 1.279													
	st.dev. (n)	0.1004													
	R(calc.)	0.281			_										
	R(ASTM D2163)	0.147			Compar	e R(EN2	27941(l	iq))=0.	732						
1.7 - 1.5 - 1.3 1.1 0.9 -		<u>▲</u> 4	▲ ▲				Δ	Δ	<u> </u>				 	 	
0.5		444	121	495 869	704	334	150	786	311	1198	463	1197	323	511	317
3.5		Ker	nel Density												
3 -		Λ													
		11													
2.5 -															
2 -															
1.5 -															
1 -															
0.5 -															
	$\wedge$ 1	l l	$\wedge$												
0 +															
0	0.5 1	1.5	2	2.5											

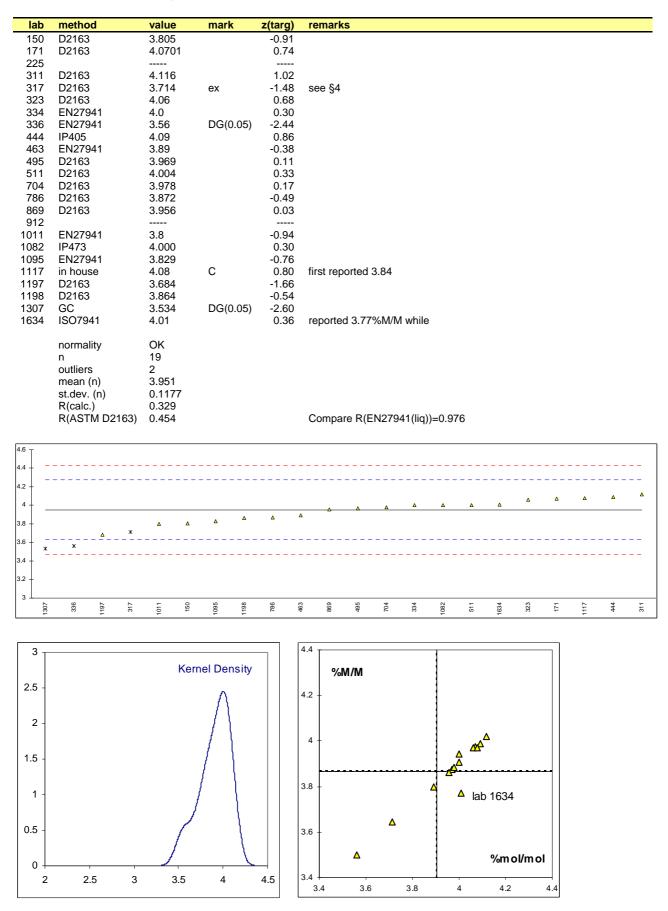
#### Determination of n-Butane; results in %mol/mol



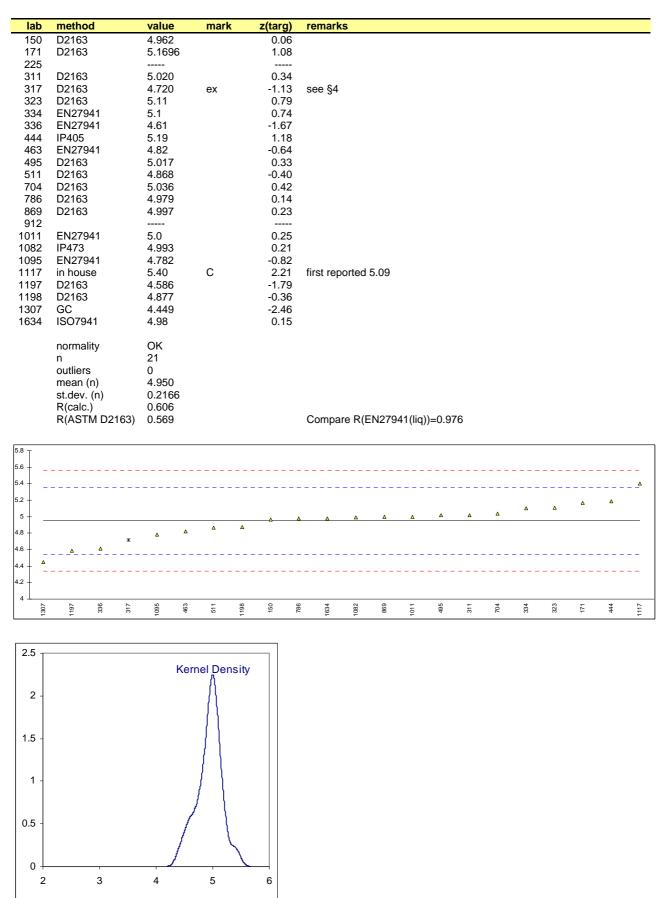
# Determination of 1,3-Butadiene; results in %mol/mol

lah	m oth o d	value	monte		romort										
lab 150	method D2163	value 0.930	mark	<b>z(targ)</b> -0.28	remark	S									
171	D2163 D2163	0.930		0.52											
225															
311	D2163	0.973		0.82											
317	D2163	0.895	ex	-1.17	see §4										
323	D2163	0.99		1.25 1.50											
334 336	EN27941 EN27941	1.0 0.84		-2.57											
444	IP405	0.97		0.74											
463	EN27941	<0.1		<-21.40	false ne	egative?									
495	D2163	0.936		-0.12											
511 704	D2163 D2163	0.894 0.937		-1.19 -0.10											
786	D2163	0.901		-1.02											
869	D2163	0.979		0.97											
912															
1011 1082	EN27941 IP473	1.0 0.948		1.50 0.18											
1082	EN27941	0.948		-1.32											
1117	in house	1.16	C,G(0.05)	5.58	first rep	orted 1.	02								
1197	D2163	0.945		0.10	•										
1198	D2163	0.905		-0.91											
1307 1634	GC ISO7941	0.839 1.04		-2.59 2.52											
1004		1.04		2.02											
	normality	OK													
	n autliana	19													
	outliers mean (n)	1 0.941													
	st.dev. (n)	0.0535													
	R(calc.)	0.150													
	R(ASTM D2163)	0.108			Compa	re R(EN	27941	(liq))=	0.941						
1.2															*
1.15 -															*
1.1 -															
1.05															
0.95							۵	۵	Δ	۵	Δ	۵	4		
0.9		*	۵ ۵	Δ	Δ Δ										_
0.85 -	A														
0.8	<u> </u>														
0.75 -															
0.7															
1307	336 336 1095 511	317	786 1198 150	495	704	1082	171	444	311	869	323	334	1011	1634	1117
7															
'		Ka	mal Danaitu												
6 -		Ke	rnel Density												
		(\													
5 -															
5		- 11													
4 -															
4 1		{	1												
3 -															
		{	{												
2 -		}													
		1	{												
1 -		1													
		1	$\bigvee$												
0	0.5			15											
0	0.5	1		1.5											
L															

#### Determination of iso-Butylene; results in %mol/mol



#### Determination of 1-Butene; results in %mol/mol



## Determination of trans-2-Butene; results in %mol/mol

lab	method		value		mark	(	z(targ)		rema	rks											
150 171	D2163 D2163		2.265 2.244				0.98 0.75														
225	D2103		Z.Z44 				0.70														
311	D2163		2.212				0.39														
317	D2163		1.860		D(0.0	05)	-3.55														
323	D2163		2.21				0.37														
334	EN27941		2.2				0.26														
336 444	EN27941 IP405		2.00 2.35				-1.98 1.94														
444 463	EN27941		2.35				-1.42														
495	D2163		2.201				0.27														
511	D2163		2.208				0.35														
704 786	D2163 D2163		2.227 2.148				0.56 -0.33														
869	D2163		2.140				0.09														
912	22100																				
1011	EN27941		2.1				-0.86														
1082	IP473		2.217				0.45														
1095 1117	EN27941 in house		2.109 2.41		С		-0.76 2.61		first r	enorte	ed 2.27	7									
1197	D2163		1.994		U		-2.05		motri	opone	, a 2.2										
1198	D2163		2.095				-0.92	2													
1307	GC		2.114				-0.71														
1634	ISO7941		2.18				0.03	5													
	normality		OK																		
	n		21																		
	outliers mean (n)		1 2.177	,																	
	st.dev. (n)		0.102																		
	R(calc.)		0.286	;																	
	R(ASTM D2	2163)	0.251						Com	oare F	R(EN2	794 <i>°</i>	1(liq)	)=0.9	76						
2.5 -																					
2.3 -																					
2.2 -										۵	۵		Δ	Δ	۵	۵	Δ	۵	۵		
2.1 -		▲	Δ	۵	۵	۵	۵														
2	<u>A</u> <u>A</u>																				
1.9																					
1.8 -																					
1.7 -																					
1.6 -																					
1.5 te	1197 336	463	1198	1011	1095	1307	786	1634	698	334	495		511	323	311	1082	704	171	150	444	1117
L	-		-	-	-	-		-								-					-
5																					
4.5 -				Kern	el Der	nsity															
4 -				Λ																	
				[]																	
3.5 -																					
3 -																					
			- 1																		
2.5 -			- 1																		
2 -																					
1.5 -			1	- {																	
				1																	
1 -			1	L																	
0.5 -		~	J		Δ																
0					1																
					0.5																

1.5

1

2

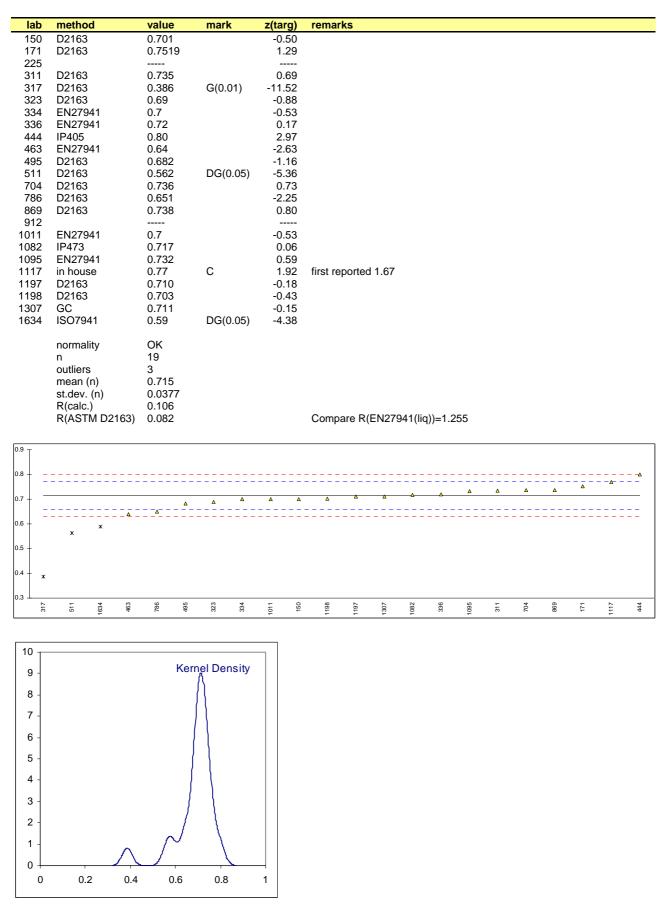
2.5

3

## Determination of cis-2-Butene; results in %mol/mol

150	method	value	mark	z(targ)	rema	rks										
150 171	D2163 D2163	1.097 1.1279		0.59 1.32												
225	22.00															
311	D2163	1.135		1.48												
317	D2163	0.865	G(0.05)	-4.82												
323	D2163	0.99		-1.90												
334 336	EN27941 EN27941	1.1 0.98		0.66 -2.14												
444	IP405	1.15		1.83												
463	EN27941	1.02		-1.20												
495	D2163	1.070		-0.04												
511 704	D2163 D2163	1.107 1.088		0.83 0.38												
786	D2163	1.039		-0.76												
869	D2163	1.097		0.59												
912																
1011	EN27941	1.0		-1.67												
1082 1095	IP473 EN27941	1.077 0.986		0.13 -2.00												
1117	in house	1.17	С	2.30	first re	eported	1.10									
1197	D2163	1.014		-1.34												
1198	D2163	1.057		-0.34												
1307 1634	GC ISO7941	1.067 1.13		-0.11 1.36												
	normality	OK														
	n outliers	21 1														
	mean (n)	1.072														
	st.dev. (n)	0.0569														
	R(calc.)	0.159			•	5 / 5										
	R(ASTM D2163)	0.123			Comp	are R(E	N279	41(liq)	)=0.97	6						
1.25 <sub>T</sub>																
1.2 -																
											۵	Δ	Δ	۵	Δ	
1.1 -				Δ	Δ Δ		Δ	Δ	۵	۵						
1.05 -		•	Δ	Δ												
1 +	<u>-</u> <u>-</u> <u>-</u> <u>-</u> - <u>-</u> <u>-</u>															
0.95 -																
0.9																
0.85 - *	ĸ															
0.8 L	336 1095 323	1011	463	1198	1307 495	1082	704	150	869	334	511	171	1634	311	444	1117
°	, e <u>6</u> e	11	4 F	5	6 4	10	~	-	00	n	a a	-	16	e	4	1
6																
		Keri	nel Density	,												
5 -			A i													
Ŭ			[]													
		1														
4 -		1														
3 -																
2 -																
-			{													
1 -			}													
		$\sim$	1													
0	1	1	L													
0	0.5	1		1.5												

#### Determination of iso-Pentane; results in %mol/mol



## Determination of iso-Butane; results in %mol/mol

<u> </u>																
lab 150	method	value	mark	z(targ)	remar	KS										
150 171	D2163 D2163	74.857 74.4030		-0.11 -1.17												
225	D2103			-1.17												
311	D2163	74.369		-1.25												
317	D2163	75.609	ex	1.65	see §4											
323	D2163	74.55		-0.83												
334	EN27941	74.4		-1.18												
336	EN27941	75.98		2.51												
444	IP405	73.95		-2.23												
463	EN27941	75.59		1.60												
495 511	D2163 D2163	74.756 73.60		-0.34 -3.04	monuo		via 1	000/		follot	horoo	mnon	onto			
704	D2163 D2163	73.60 74.523		-3.04 -0.89	manua	any care	. via i	00%-	Sum O	i ali ul		mpon	ents			
786	D2163	74.596		-0.72												
869	D2163	74.349		-1.29												
912																
1011	EN27941	75.4		1.16												
1082	IP473	74.678		-0.53												
1095	EN27941	75.943		2.42												
1117	in house	74.06	С	-1.97	first rep	ported	74.87									
1197	D2163	75.337		1.01												
1198 1307	D2163 GC	74.445 75.690		-1.07 1.83												
1634	ISO7941	76.20		3.02												
1004				0.02												
	normality	OK														
	n	20														
	outliers	1														
	mean (n)	74.904														
	st.dev. (n) R(calc.)	0.6810 1.907														
	R(ASTM D2163)	1.200			Compa	are R/F	N279/	41(lia)	$)-15^{\prime}$	16						
		1.200			Compe		11210	(	)=1.0							
76.5 <sub>T</sub>																
																<b>Δ</b>
76 -														Δ	Δ	
75.5 -											۵	ж	Δ			
									۵	Δ						
75 -								Δ								
74.5				<u>م</u>	Δ Δ	۵	۵									
	<u>۸</u>	Δ Δ	Δ	-												
74	Δ															
73.5 *	<b>*</b>															
73	444	311 334	171	704	323 786	1082	495	150	1197	1011	463	317	1307	1095	336	1634
с. 	0 4 5 0	e e	-	4 1	ю r	10	4	÷	-	10	4	e	13	10	e	16
0.6 –																
0.0		Kaa		14.												
	(		nel Dens	ity												
0.5 -		1														
		1														
		1														
0.4 -	)															
0.3 -		$\sim$														
		- \														
		Y	1													
0.2 -	/		\													
			1													
0.1 -	1		$\lambda$													
0.1 -	1		1													
			$\langle \rangle$													
o  -			<u> </u>													
72	74	76	6	78												

### Determination of Molar Mass; results in g/mol

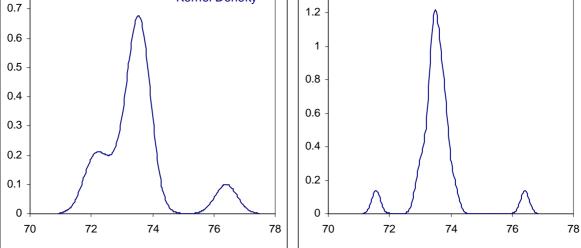
	mination of N			
lab	method	value	mark	remarks
150 171 225 311 317 323 336 444 463 495 511 704 786 869 912 1011 1082 1095	in house D2598	57.440 57.48 57.4 57.4 57.4 57.4 56.69 57.4633 57.438 57.46 57.46 57.46 57.73	G(0.05) D(0.05)	       Calculated by iis from the reported test results: 57.46
1197 1198 1307 1634	normality n outliers mean (n) st.dev. (n) R(calc.) R(lit)	not OK 7 2 57.406 0.1020 0.286 unknown		 Calculated by iis from all reported test results: OK 18 4 57.465 0.0381 0.107 unknown
58         57.8         57.6         57.7         56.8         56.6         56.4         56.2         56	88 X	312	<b>∆</b> 82 82	 311 200 1117 701 1117 701 1117 701 1117
4 - 3.5 - 3 - 2.5 - 2 - 1.5 - 1 - 0.5 - 0 - 5	6 56.5	57	Kernel I	$\begin{array}{c} 8 \\ 7 \\ 6 \\ 5 \\ 4 \\ 3 \\ 2 \\ 1 \\ 0 \\ 58.5 \end{array}$

#### Determination of Relative Density @ 60F; unitless results

		n of F	Relative I					sults						
lab	method		value	mark	z(targ)	rema	arks							
150	D2598		0.5694											
171	D2598		0.56933											
225 311	D2598		 0.5691											
317	D2330 D2421		0.5674	G(0.01)										
323	D2598		0.5690	0(0.01)										
334	22000													
336														
444														
	ISO8973		0.5686											
495 511	D2598 D2598		0.569652 0.5690											
	D2598		0.5691											
	D2598		0.5689											
	D2163		0.5692											
912														
1011	D2598		0.5691											
1095	D2330													
1117	calc.		0.5700											
1197														
1198														
1307 1634	ISO8973		0.5696											
1004	1000910		0.0090			Calc	ulated by	iis from	all reporte	d test res	sults:			
	normality		ОК			OK					<u> </u>			
	n		13			20								
	outliers		1			2	20							
	mean (n) st.dev. (n)		0.5692 0.00037			0.569								
	R(calc.)		0.0010			0.00								
	R(lit)		unknown			unkn								
0.5706 T														
0.5701 -														
													*	۵
0.5696 -										۵	۵	۵	*	
0.5691 -			۵	Δ	Δ .	Δ	Δ	Δ	∆					
0.5686 -		4												
0.5681 -														
0.5676 -	ж													
0.5671 -														
0.5666														
	317	463	786	323	511	Ş	1082	311	869	171	150	1634	495	1117
400														1
1200	,					ηl	1400	0-1	bulle &	and all a	با- مشم		to 1	
				Kernel	Density				. by its fro	om all re	ported	test resul	ເຮ	
1000	) _			$\Lambda$			1200	-			Λ			
											( )			
							1000	4						
800	) -			$\left( \right)$										
				$  \rangle$			800				$  \rangle$			
000				$  \rangle$							$  \rangle$			
600	1													
							600	1						
400	) -		(	\\							$  \rangle$			
							400	-						
					λ						/ \	~~~		
200	) -		1		$\backslash$		200	1			(	$\sqrt{\gamma}$		
		$\wedge$			$\mathbf{X}$				$\sim$					
		)	$\bigvee$				0							
		567	0.569 0			574		566		569		0.57		
	0.566 0.	567	0.568 0	).569 C	).57 0.	571	0.	566	Ĺ	).568		0.57		
							L							J

## Determination of Abs. Vapour Pressure; results in psi

		OT A				esults in	psi					
lab	method		value	mark		remarks						
	IP432		73.6	С		first reporte						
171	D2598		72.0036			Calculated	by its from t	ne reporte	ed test resu	lts: 73.17 psi		
225 311	D2598		 73.6									
317	ISO8973		73.0 76.4	G(0.01)								
323	1000975			0(0.01)								
334												
336												
444												
463	ISO8973		73.6752									
495	D2598		72.23			Calculated	by iis from t	he reporte	ed test resu	lts: 73.44 psi		
511												
704	ISO8973		73.45									
786	ISO8973		73.699									
869	D2163		72.8									
912												
1011 1082	ISO8973		 73.436									
1082	1000910		73.430									
1117												
1197												
1198												
1307												
1634												
							by iis from a	Il reported	d test result	<u>s:</u>		
	normality		not OK			OK						
	n		10			18						
	outliers		1			2						
	mean (n)		73.19			73.52 0.296						
	st.dev. (n) R(calc.)		0.622 1.74			0.290						
	R(lit)		unknown			unknown						
	r (iii)		anatom			unatown						
77 <sub>T</sub>												
l''⊺												
76 -												ж
75 -												
74 -												
				۵		۵	Δ	۵	Δ	۵	۵	
73 -			Δ									
70		Δ	_									
72 -	Δ											
71 -												
70	5	495	869	ĸ		8	704	5	150	463	786	1
	4	4	86	1095		1082	Ň	31,	¥	4	7	317
0.8						1.4						7
0.0						'.4	Calc	hvije fro	m all repo	orted test re	sulte	
				Kernel [	Density			5915110	in an iept		Juno	
0.7	1		^			1.2	-		۸			
			/ \						- 11			



#### Determination of Rel. Vapour Pressure; results in psi

Ibb         method         value         mark         igging         remarks           150         D2598         65.7.656		mination of F				
171 D2598   57.656			value	mark		
$ \frac{311}{317} = \frac{312}{314} =$	171		57.656			
		D2598				-
$ \frac{334}{443} = \frac{1}{12} + \frac{1}{$	317					-
$ \frac{336}{44}   P432 \\ \frac{344}{45}   P432 \\ \frac{356}{57.53} \\ \frac{357}{10}   5268 \\ \frac{357.53}{57.53} \\ \frac{357}{10}   526973 \\ \frac{356.1}{57.53} \\ \frac{357}{10} \\ \frac{357}{10}$						-
444       IP432       58.0       C						
$ \begin{array}{cccccccccccccccccccccccccccccccccccc$	444	IP432		С		- first reported <u>Abs</u> . Vapour Pressure 58.0
$ \begin{array}{cccccccccccccccccccccccccccccccccccc$		Docoo				
$ \begin{array}{cccccccccccccccccccccccccccccccccccc$						•
$ \begin{array}{cccccccccccccccccccccccccccccccccccc$	704	ISO8973	58.76			-
912						-
$1011 \qquad \qquad \qquad \\ 1082 \qquad \qquad \\ 1177 \qquad \qquad \\ 1188 \qquad \qquad \\ 1189 \qquad \qquad \\ 1180 \qquad$		D2163				-
$1035 \\ 1117 \\ 1117 \\ 1138 \\ 1138 \\ 1138 \\ 1138 \\ 1139 \\ $	1011					-
$1117 \qquad \dots \qquad \dots \\ 1197 \qquad \dots \qquad \dots \\ 1197 \qquad \dots \qquad \dots \\ 100 \qquad 100 \qquad \dots \\ 100 \qquad 10 \qquad 0 \\ 10 \qquad 10 \qquad 0 \\ 10 \qquad 10 \qquad$						-
$137 \qquad \dots \qquad \dots \\ 138 \qquad \dots \qquad \dots \\ 137 \qquad \dots \qquad \dots \\ 138 \qquad \dots \qquad \dots \\ 138 \qquad \dots \qquad \dots \\ 138 $	1095		58.1			-
$1307 \qquad \\ 1634   SO2073 \qquad 60.626  G(0.05) \qquad \\ normality \qquad OK \qquad & 10 & 13 \\ outliers & 1 & 2 \\ mean (n) & 58.28 & 58.82 \\ st.dev. (n) & 0.524 & 0.296 \\ R(cat.) & 1.47 & 0.03 \\ mean (n) & unknown & unknown \\ \hline \\ $	1197					-
$1634 \  SC8973 \\ normality OK \\ mean (n) \\ st.dev. (n) \\ (listronov line (listronov list from all reported test results:  mean (n) \\ st.dev. (n) \\ st.dev$						-
$ \begin{array}{c c} \begin{array}{c} \begin{array}{c} \begin{array}{c} \begin{array}{c} \begin{array}{c} \begin{array}{c} \begin{array}{c} \begin{array}{$	1634	ISO8973		G(0.05)		
n = 10 = 18 = 2 = 28 = 58.82 = 58.82 = 58.82 = 0.233			<b></b>	, ,		Calculated by iis from all reported test results:
outliers       1       2         mean (n)       58.28       58.82         st.dev. (n)       0.524       0.296         R(catc.)       1.47       0.83         generation       a       a         a       a       a         a       a       a         a       a       a         a       a       a         a       a       a         a       a       a         a       a       a         a       a       a         a       a       a         b       E       3       B </td <td></td> <td></td> <td></td> <td></td> <td></td> <td></td>						
$\begin{array}{c ccccccccccccccccccccccccccccccccccc$			1			2
$\begin{array}{c ccccccccccccccccccccccccccccccccccc$		mean (n)				
R(iii) unknown unknown $x$		st.dev. (n) R(calc.)				
$ \begin{array}{c} & & & & & & \\ & & & & & \\ & & & & & \\ & & & & \\ & & & & \\ & & & & \\ & & & & \\ & & & & \\ & & & \\ & & & & \\ & & & & \\ & & & \\ & & & \\ & & & \\ & & & \\ & & & \\ & & & & \\ & & & \\ $		R(lit)				
$ \begin{array}{c} & & & & & & \\ & & & & & & \\ & & & & & & & \\ & & & & & & \\ & & & & & & & \\ & & & & & & \\ & & & & & & & \\ & $						
$ \begin{array}{c} \begin{array}{c} \begin{array}{c} \begin{array}{c} \begin{array}{c} \end{array}{0.5}\\ \end{array}{0.5}\\ \end{array}{0.5}\\ \end{array}{0.5}\\ \end{array}{0.7}\\ \end{array}{0.7}\\ \end{array}{0.7}\\ 0.4\\ 0.3\\ 0.2\\ 0.1\\ \end{array}{0.7}\\ \end{array}{0.7}\\ 0.4\\ 0.2\\ 0.4\\ 0.2\\ \end{array}{0.7}\\ 0.4\\ 0.4\\ 0.2\\ 0.4\\ 0.4\\ 0.2\\ 0.4\\ 0.4\\ 0.2\\ 0.4\\ 0.4\\ 0.4\\ 0.2\\ 0.4\\ 0.4\\ 0.4\\ 0.2\\ 0.4\\ 0.4\\ 0.4\\ 0.2\\ 0.4\\ 0.4\\ 0.4\\ 0.2\\ 0.4\\ 0.4\\ 0.4\\ 0.4\\ 0.4\\ 0.4\\ 0.2\\ 0.4\\ 0.4\\ 0.4\\ 0.4\\ 0.4\\ 0.4\\ 0.4\\ 0.4$	61 T					
$ \begin{bmatrix} 395 \\ 995 \\ 985 \\ 985 \\ 98 \\ 98 \\ 98 \\ 98$	60.5 -					X
$ \begin{bmatrix} 39 \\ 585 \\ 587 \\ 57 \\ 9 \\ 57 \\ 9 \\ 57 \\ 9 \\ 57 \\ 9 \\ 57 \\ 9 \\ 57 \\ 9 \\ 57 \\ 9 \\ 57 \\ 9 \\ 57 \\ 9 \\ 57 \\ 9 \\ 57 \\ 9 \\ 57 \\ 9 \\ 57 \\ 9 \\ 57 \\ 9 \\ 57 \\ 9 \\ 57 \\ 9 \\ 57 \\ 9 \\ 57 \\ 9 \\ 9 \\ 9 \\ 9 \\ 9 \\ 9 \\ 9 \\ 9 \\ 9 \\ $	60 -					
$ \begin{array}{c}                                     $	59.5 -					
$ \begin{array}{c} \begin{array}{c} \begin{array}{c} \begin{array}{c} \begin{array}{c} \begin{array}{c} \end{array} \\ \end{array} \\ \begin{array}{c} \end{array} \\ \begin{array}{c} \end{array} \\ \begin{array}{c} \end{array} \\ \end{array} \\ \end{array} \\ \begin{array}{c} \end{array} \\ \end{array} \\ \begin{array}{c} \end{array} \\ \end{array} \\ \end{array} \\ \begin{array}{c} \end{array} \\ \end{array} \\ \end{array} \\ \begin{array}{c} \end{array} \\ \end{array} \\ \end{array} \\ \end{array} \\ \begin{array}{c} \end{array} \\ \end{array} \\ \end{array} \\ \end{array} \\ \end{array} \\ \begin{array}{c} \end{array} \\ \begin{array}{c} \end{array} \\ \end{array} \\$	59 -					
$\begin{bmatrix} 0.6 \\ 0.5 \\ 0.4 \\ 0.3 \\ 0.2 \\ 0.1 \end{bmatrix}$ $\begin{bmatrix} 0.6 \\ 0.6 \\ 0.6 \\ 0.4 \\ 0.1 \end{bmatrix}$ $\begin{bmatrix} 1.4 \\ 1.2 \\ 1 \\ 0.8 \\ 0.6 \\ 0.4 \\ 0.2 \end{bmatrix}$ $\begin{bmatrix} 1.4 \\ 1.2 \\ 1 \\ 0.8 \\ 0.6 \\ 0.4 \\ 0.2 \end{bmatrix}$ $\begin{bmatrix} 0.6 \\ 0.4 \\ 0.4 \\ 0.2 \end{bmatrix}$	58.5 -					Δ Δ
$ \begin{array}{c} 57.5 \\ 57 \\ \hline 8 \\ 8 \\ 8 \\ \hline 8 \\ 8 \\ 8 \\ 8 \\ 8 \\ 8 \\ 8 \\ 8 \\ 8 \\ 8 \\$	58 -		Δ	۵		Δ Δ
$\begin{bmatrix} 57 \\ \hline $		<u>م</u>				
$ \begin{array}{c ccccccccccccccccccccccccccccccccccc$						
Kernel Density       Calc. by iis from all reported test results         0.5       1.2         0.4       1         0.3       0.8         0.2       0.6         0.1       0.4	0.	495	444	511		1095 869 704 704 705 7150
Kernel Density       Calc. by iis from all reported test results         0.5 -       .4 -         0.3 -       .1 -         0.2 -       .6 -         0.1 -       .2 -         0.1 -       .2 -	L					
Kernel Density       Calc. by iis from all reported test results         0.5 -       .4 -         0.3 -       .1 -         0.2 -       .6 -         0.1 -       .2 -         0.1 -       .2 -	0.6					
0.5     0.4     1.2       0.3     0.8       0.2     0.4       0.1     0.2	0.0 -					
$ \begin{array}{cccccccccccccccccccccccccccccccccccc$				Kerner L	Density	
0.4 -       0.3 -       0.8 -       0.6 -         0.2 -       0.4 -       0.4 -       0.6 -         0.1 -       0.2 -       0.4 -       0.4 -	0.5 -					
0.4 -       0.3 -       0.8 -       0.6 -         0.2 -       0.4 -       0.4 -       0.6 -         0.1 -       0.2 -       0.4 -       0.4 -			<b>`</b>			
	0.4 -		\			
	03.					
	0.0					
	0.2 -					
	0.1 -			$\sim$		
		}	$ \setminus /$	$\backslash$		
	0 -			<u> </u>		
56 58 60 62 64 56 58 60 62 64		6 58	60	62		

#### Additional details

	Sample Volume	Type of vaporizer	Remarks
150			C6+ 0.005 %mol/mol
171			n-pentane: 0.0037 %mol/mol (0.0044 %M/M)
225			
311			n-pentane: 0.0037 %mol/mol & helium 0.45 %mol/mol
317	0.1 mL	none, liquid injection	none
323	190 mL	none, liquid injection	none
334			none
336			
444		none, liquid injection	sample for one injection only, n-pentane <0.01 %mol/mol
463	45 mL		
495	202 mL	waterbath	n-pentane trace & helium 1.4 %mol/mol (0.05 %M/M)
511			
704	0.0005 mL	SPL	n-pentane: 0.004 %M/M (0.003 %mol/mol)
786			
869	0.2 µL	none, liquid injection	n-pentane: 0.003 %mol/mol
912			
1011			none
1082	0.1 µL	none, liquid injection	n-pentane: 0.003 %M/M
1095	20.1 grams	vaporised at RT	
1117	18.1 mL	LSV	iso-butane and propene co-elute
1197		GSV with heater	n-pentane: 0.003695 %mol/mol
1198		GSV with heater	n-pentane: 0.003539 %mol/mol
1307			
1634			none

#### List of participants

SGS Belgium N.V OGC	Antwerp	BELGIUM
FINA Antwerp Olefins	Antwerp	BELGIUM
SGS Cote d'Ivoire S.A.	Abidjan	CÔTE D'IVOIRE
Neste Oil Oyj, Development and Laboratories	Porvoo	FINLAND
SGS France S.A.	Lavera	FRANCE
SGS France S.A. (Donges)	Montoir de Bretagne	FRANCE
SGS Germany GmbH	Wilhelmshaven	GERMANY
M/S SGS India Pvty Ltd.	Thane, Mumbai	INDIA
Petronas Gas Berhad - laboratory GPPA	Kerteh, Kemamn, Terengganu	MALAYSIA
Petronas Gas Berhad - laboratory GPPB	Kerteh, Kemamn, Terengganu	MALAYSIA
SGS-CSTC Standards Technical Services Ltd., Zhuhai branch	Shenzhen	P.R. of CHINA
SGS Del Peru S.A.C.	Callao	PERU
GalpEnergia / Petrogal S.A Refinaria do Porto – Laboratorio	Leça da Palmeira	PORTUGAL
GalpEnergia / Petrogal S.A Refinaria de Sines - Laboratorio	Sines	PORTUGAL
Companhia Logistica de Combustiveis S.A.	Azambuja	PORTUGAL
ZAO "SGS Vostok Ltd", Temruk branch	Temryuk, Krasnodar Region	RUSSIA
SGS Sweden AB	Göteborg	SWEDEN
SGS Nederland BV - OGC	Spijkenisse	THE NETHERLANDS
SGS Nederland BV	Vlissingen	THE NETHERLANDS
Shell Ned. Chemie B.V., Clab/3	Moerdijk	THE NETHERLANDS
SGS New Orleans (St. Rose)	New Orleans	U.S.A.
SGS Deer Park	Deer Park	U.S.A.
SGS Ukraine Ltd., Odessa branch	Odessa	UKRAINE
SGS (UK) Ltd., Billingham branch (Teesside)	Billingham, Cleveland	UNITED KINGDOM

#### Abbreviations:

- C = final result after checking of first reported suspect result
- D(0.01) = outlier in Dixon's outlier test
- D(0.05) = straggler in Dixon's outlier test
- G(0.01) = outlier in Grubbs' outlier test
- G(0.05) = straggler in Grubbs' outlier test
- DG(0.01) = outlier in Double Grubbs' outlier test
- DG(0.05) = straggler in Double Grubbs' outlier test
- ex = excluded from calculations
- n/a = not applicable
- W = withdrawn on request participant
- U = reported in wrong unit
- E = error in calculations
- SDS = Safety Data Sheet

#### Literature:

- 1 iis Interlaboratory Studies, Protocol for the Organisation, Statistics and Evaluation, January 2010
- 2 prNEN 12766-2:2000.
- 3 ASTM E178-89
- 4 ASTM E1301-89
- 5 ISO 5725-86
- 6 ISO 5725, parts 1-6, 1994
- 7 M. Thompson and R. Wood, J. AOAC Int, <u>76</u>, 926, (1993)
- 8 W.J. Youden and E.H. Steiner, Statistical Manual of the AOAC, (1975)
- 9 IP 367/84
- 10 DIN 38402 T41/42
- 11 P.L. Davies, First reported Z. Anal. Chem, <u>331</u>, 513, (1988)
- 12 J.N. Miller, Analyst, <u>118</u>, 455, (1993)
- 13 Analytical Methods Committee Technical Brief, No4 January 2001
- 14 The Royal Society of Chemistry 2002, Analyst 2002, 127 page1359-1364, P.J. Lowthian and M. Thompson. (see <u>http://www.rsc.org/suppdata/an/b2/b205600n/</u>)
- 15 ISO 17043
- 16 EN 27941
- 17 ASTM D2163
- 18 ASTM D2421